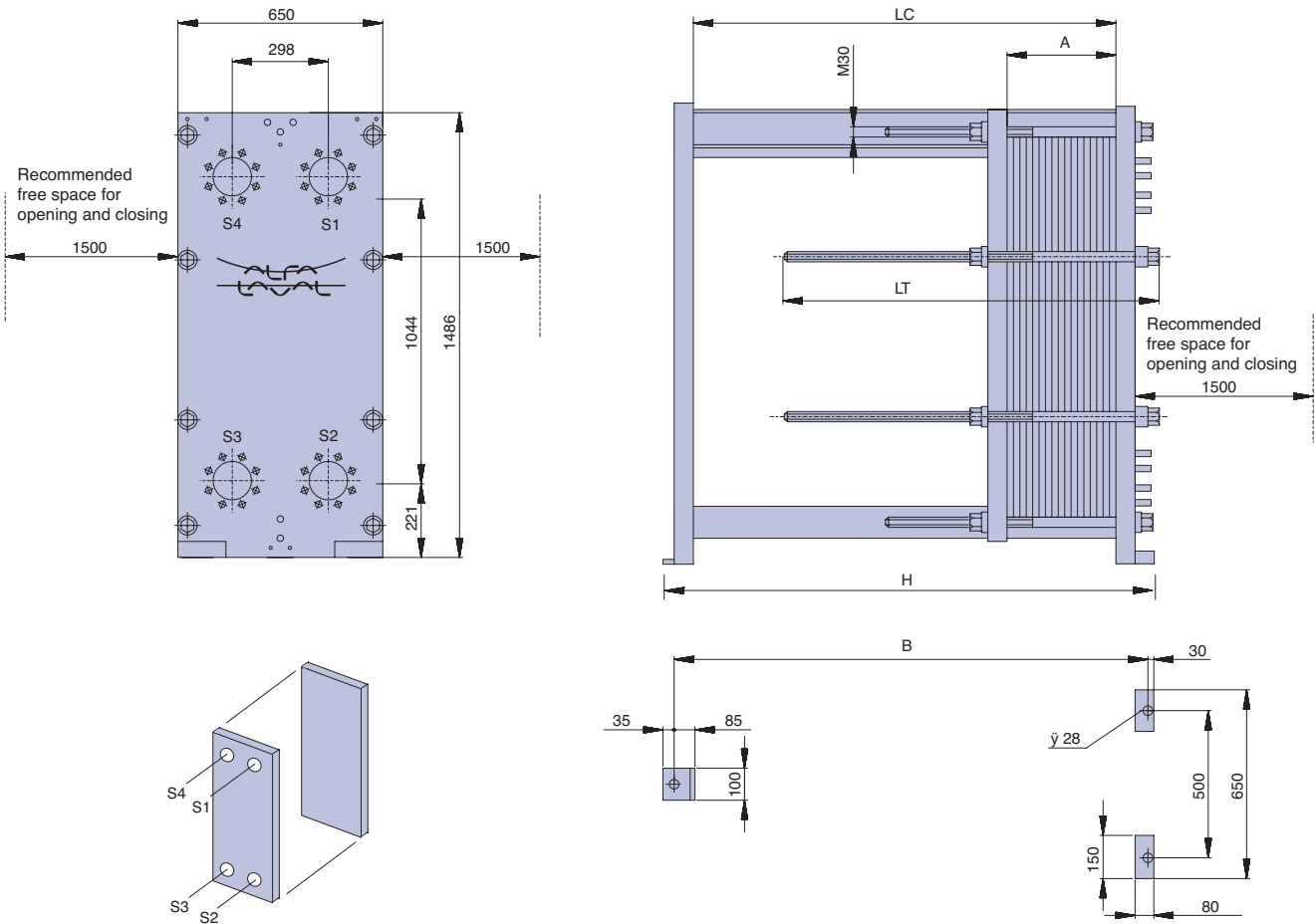


N° of cassetts			30	40	50	60	70	80
Nominal data Ethylene Glycol = 30% Ti = -2°C To = -6°C Refrigerant = NH <sub>3</sub> Te = -10°C	Qn	kW	340	460	580	690	800	900
	Wn	m <sup>3</sup> /h	83,2	112,6	142,0	168,9	195,8	220,3
	Δp glycol	bar	0,90	0,92	0,94	0,96	0,96	0,97
	Δp NH <sub>3</sub>	kPa	6,8	7,0	7,2	7,3	7,4	7,5



N° of cassetts, 0,6 mm			< 37	< 66	< 94	< 121	< 179	< 215
DIMENSIONS	A	mm	229	409	583	750	1100	1333
	Lc	mm	900	1200	1500	1800	2400	2800
	Lt	mm	750	1050	1350	1650	2250	2850
	H	mm	1200	1500	1800	2100	2700	3100
	B	mm	1095	1395	1695	1995	2595	2995
	Connection	mm	DN 150	DN 150	DN 150	DN 150	DN 150	DN 150
DATA	V <sub>H<sub>2</sub>O</sub>	dm <sup>3</sup>	44,4	81,3	116,8	151,1	224,8	270,5
	V <sub>NH<sub>3</sub></sub>	dm <sup>3</sup>	45,7	82,6	118,1	152,4	226,1	271,8
	W <sub>0</sub>	Kg	1190	1420	1640	1850	2300	2540

<b>S1</b> Outlet water	<b>Ti</b> Glycol inlet temperature	<b>Wn</b> Glycol nominal flow	<b>V H<sub>2</sub>O</b> Water volume
<b>S2</b> Inlet water	<b>Tu</b> Glycol outlet temperature	<b>Δp glycol</b> Glycol pressure drop	<b>V NH<sub>3</sub></b> Ammonia volume
<b>S3</b> Inlet refrigerant	<b>Te</b> Evaporation temperature	<b>Δp NH<sub>3</sub></b> Ammonia pressure drop	
<b>S4</b> Outlet refrigerant	<b>Qn</b> Nominal capacity	<b>W<sub>0</sub></b> Operating weight	